# Simulation of surfactant in diffuse interface flow

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Flashes on research in scientific computing Uppsala, November 24, 2010

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#### Joint work

The Linné FLOW center, Micro- and complex fluids group

#### Gustav Amberg, Minh Do-Quang, and Anna-Karin Tornberg

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# Outline

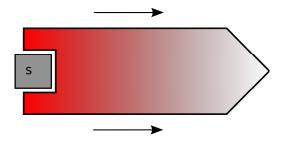
- Motivation: surfactants in fluid mixtures
- Diffuse interface modeling; the Ginzburg-Landau energy
- Diffuse interface modeling of surfactant two-phase flow
- Numerical illustrations and surprises

# Motivation

Surface active agents:

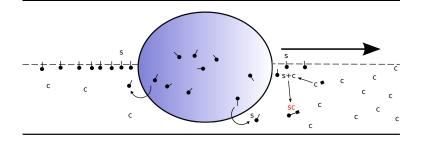
- Surfactants main usage comes from the fact that they lower the surface tension of liquid interfaces.
- Surfactants may therefore act as: detergents, wetting agents, emulsifiers (in food!), foaming agents, and dispersants (preventing settling or clumping in suspensions).

# The soapraft



Realized very recently *in vivo* (Lagzi *et. al, J. Am. Chem. Soc.* (2010)) [maze.avi]

The maze solving droplet



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# Phase-field modeling

- Case: two immiscible fluids (eg. oil/water).
- Introduce the phase-field variable φ which is ±1 in the two liquids, *diffuse* interface understood at φ = 0.
- Goal: formulate a PDE in φ given thermodynamic potentials of the system (guess/ansatz/heuristics).

Phase-field modeling (cont.)

Non-dimensional Ginzburg-Landau free energy:

$$F_{\phi} = \int_V f(\phi) + rac{\operatorname{Cn}^2}{4} (
abla \phi)^2 \, dV,$$

with the standard choice  $f(\phi) = (1 - \phi)^2 (1 + \phi)^2$ , a "double well" potential with two equilibrium states at  $\phi = \pm 1$ . But this is clearly not unique!

-Have also introduced the single parameter Cn, the Cahn number

(i.e. the non-dimensional thickness of the interface).

# Phase-field modeling (cont.)

Take the variation (functional derivative) of  $F_{\phi}$  wrt.  $\phi$ ,

$$rac{\delta \mathcal{F}_{\phi}}{\delta \phi} = f'(\phi) - rac{\mathsf{Cn}}{2} \Delta \phi =: \mu_{\phi} \quad ( ext{chemical potential}).$$

A suitable PDE for  $\phi$  is now

$$\frac{\partial \phi}{\partial t} = \nabla \cdot M_{\phi} \nabla \mu_{\phi}$$
 (Cahn-Hilliard equation),

plus appropriate BCs. *Note:* the mobility  $M_{\phi}$  need not be constant! -In practice: couple this to a flow field **u** driven eg. by the Navier-Stokes equations.

### Phase-field modeling: pros and cons

- + Takes care of arbitrary topological changes at the cost of an implicit and diffuse interface.
- +/- Phenomenological: "A theory which expresses mathematically the results of observed phenomena without paying detailed attention to their fundamental significance" (Concise Dictionary of Physics (1973)). Some philosophers of science (Cartwright (1984)) argue that all laws of Nature are phenomenological generalizations...
- +/- "Straightforward" to generate new equations to account for new situations.
  - The numerical resolution near the interface where  $\phi \approx 0$  may have to be *very* thin in order to capture the correct dynamics.

## Phase field modeling of surfactants

- Two immiscible fluids (eg. oil/water) plus a surfactant (eg. a detergent).
- ► Phase-field variable φ as before, new variable ψ ∈ [0, 1] is the concentration of surfactant.

Suggested Ginzburg-Landau free energy

$$\begin{split} F &= F_{\phi} + \int_{V} F_{\psi} + F_{1} + F_{ex} \, dV, \\ F_{\psi} &= \mathsf{Pi} \left[ \psi \log \psi + (1 - \psi) \log(1 - \psi) \right], \quad (\mathsf{a.k.a. diffusion!}) \\ F_{1} &= -\frac{\mathsf{Cn}^{2}}{4} \psi (\nabla \phi)^{2}, \\ F_{ex} &= \frac{1}{4 \operatorname{Ex}} \psi \phi^{2}. \end{split}$$

(van der Sman et. al, Rheol. Acta (2006))

## Phase field+surfactants (cont.)

The variation of F wrt.  $\phi$  and  $\psi$  (chemical potentials),

$$\frac{\delta F}{\delta \phi} = \ldots =: \mu_{\phi}, \quad \frac{\delta F}{\delta \psi} = \ldots =: \mu_{\psi}.$$

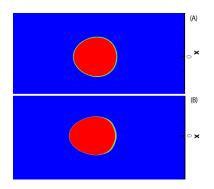
A suitable system of PDEs is now

$$\begin{aligned} \phi_t + \nabla \cdot (\phi \mathbf{u}) &= \nabla \cdot M_{\phi} \nabla \mu_{\phi}, \\ \psi_t + \nabla \cdot (\psi \mathbf{u}) &= \nabla \cdot M_{\psi} \nabla \mu_{\psi}, \\ \rho_t + \nabla \cdot (\rho \mathbf{u}) &= 0, \end{aligned}$$
$$\rho \left( \mathbf{u}_t + \mathbf{u} \cdot \nabla \mathbf{u} \right) &= -\nabla P(\phi, \psi) + \frac{1}{\text{Re}} \nabla \cdot \left( \rho \nu [\nabla \mathbf{u} + \nabla \mathbf{u}^T] \right). \end{aligned}$$

(van der Sman et. al, Rheol. Acta (2006))

### Illustrations 1

- Multiple time-scales [phases.gif]
- Merging/bouncing bubbles [withoutsurf\_phi.mov, withsurf\_phi.mov, withsurf\_psi.mov] (simulations by Minh Do-Quang)



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### The Langmuir isotherm

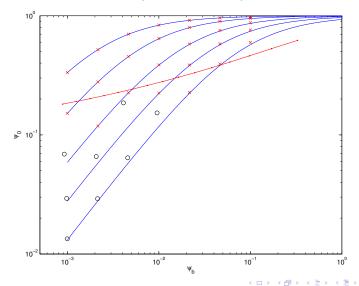
At equilibrium we must have  $\mu_{\psi_0} = \mu_{\psi_b}$ , i.e. the chemical potential is the same in the interface  $\psi_0$  and in the bulk  $\psi_b$ . Surprisingly, this relation can be solved up to order  $O(\psi_b)$ ,

$$\psi_0 = \frac{\psi_b}{\psi_b + \psi_c}$$

the Langmuir isotherm, with  $\psi_c$  the Langmuir constant. Possessing an isotherm is a strength as  $\psi_c$  can be measured. (van der Sman *et. al, Rheol. Acta* (2006))

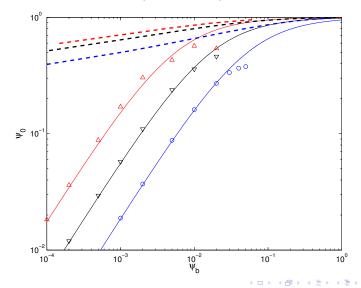
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# The Langmuir isotherm (1D, spectral)



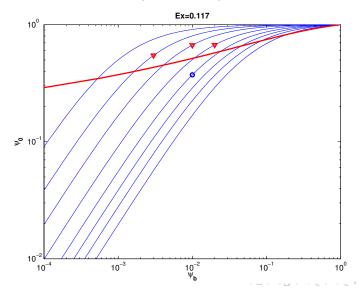
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The Langmuir isotherm (1D, FEM)



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# The Langmuir isotherm (2D, FEM)



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#### III-posedness

Free-space problem in 1D with  $\mathbf{u} = 0$ . Make the perturbed equilibrium ansatz  $\phi = \phi_{\infty} + \delta u$  and  $\psi = \psi_{\infty} + \delta v$ . The principal part is

$$\begin{bmatrix} u_t \\ v_t \end{bmatrix} = \begin{bmatrix} -\frac{Cn^2}{2} \frac{1-\psi_{\infty}}{Pe_{\phi}} D^4 & \frac{Cn^2}{2} \frac{D(\phi_{\infty})}{Pe_{\phi}} D^3 \\ -\frac{Cn^2}{2} \frac{\psi_{\infty}(1-\psi_{\infty})D(\phi_{\infty})}{Pe_{\psi}} D^3 & \frac{Pi}{Pe_{\psi}} D^2 \end{bmatrix} \begin{bmatrix} u \\ v \end{bmatrix}$$

"Frozen coefficient" Fourier transform (  $D=d/dx
ightarrow-i\omega$  ),

$$\begin{bmatrix} \hat{u}_t \\ \hat{v}_t \end{bmatrix} = \begin{bmatrix} -\frac{Cn^2}{2} \frac{1-\psi_{\infty}}{Pe_{\phi}} \omega^4 & \frac{Cn^2}{2} \frac{D(\phi_{\infty})}{Pe_{\phi}} i \omega^3 \\ -\frac{Cn^2}{2} \frac{\psi_{\infty}(1-\psi_{\infty})D(\phi_{\infty})}{Pe_{\psi}} i \omega^3 & -\frac{Pi}{Pe_{\psi}} \omega^2 \end{bmatrix} \begin{bmatrix} \hat{u} \\ \hat{v} \end{bmatrix}.$$

Calculations show that there is an eigenvalue

$$\lambda_2 = rac{1}{\mathsf{Pe}_\psi} \left[ rac{\mathsf{Cn}^2}{2} \psi_\infty (D(\phi_\infty))^2 - \mathsf{Pi} 
ight] \omega^2 + O(1).$$

Unphysical instability whenever  $\lambda_2 > 0!$ 

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# Illustrations 2

An approximate sufficient condition for instability is

$$\mathsf{Pi} < \frac{\psi_0}{2} \approx \frac{1}{2} \frac{\psi_b}{\psi_c + \psi_b}.$$

[explosion\_refined0.gif]

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#### Well-posedness

The PDE for  $\phi$  is 4th order, for  $\psi$  2nd order... Coupling through the two energy terms

$$\begin{split} F_1 &= -\frac{\mathsf{Cn}^2}{4}\psi(\nabla\phi)^2,\\ F_{\mathrm{ex}} &= \frac{1}{4\,\mathsf{Ex}}\psi\phi^2, \end{split}$$

where the former is in fact a diffuse version of a sharp term,

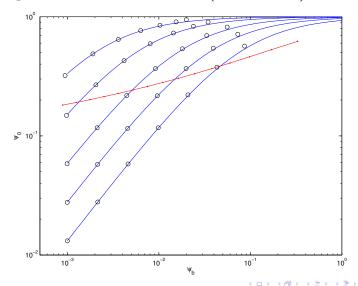
$$F_1 pprox -rac{\psi}{4} \cdot \delta_{ ext{interface}}.$$

A simple solution is to prefer  $F_1 = -\psi/4 \cdot (1 - \phi^2)$ . One can show that this does not change the isotherm.

# Conclusions

- Surfactants and modeling of them through diffuse interfaces.
- Numerical simulations show qualitatively the correct behavior (bouncing bubbles, Langmuir isotherm).
- Result: conditional unphysical instability.
- Simple fix to this. [explosion\_refined.gif]

## The Langmuir isotherm revisited (new model)



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